

# JOHNSON GAS APPLIANCE COMPANY TEST REPORT

## SCOPE OF WORK

EPA EMISSIONS TESTING FOR MODEL ELEMENT-P II PELLET FUEL ROOM HEATER

## REPORT NUMBER

105164443MID-005R2

## TEST DATE(S)

10/26/22

## ISSUE DATE

10/31/22

## [REVISED DATE]

11/09/23

## PAGES

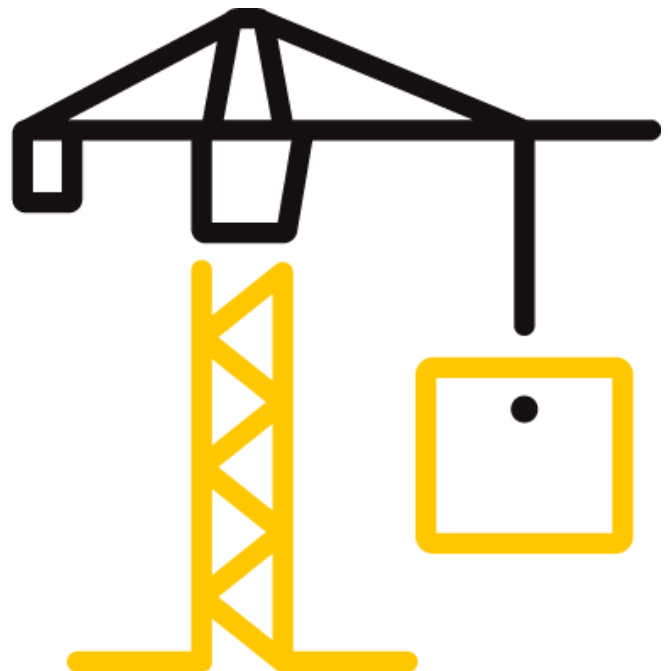
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## TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY

Report No.: 105164443MID-005R2

Date: 11/09/23

### REPORT ISSUED TO

#### JOHNSON GAS APPLIANCE COMPANY

1155 Sherman Road  
Hiawatha, IA 52233

### SECTION 1

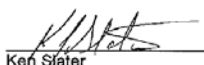
#### SCOPE

Intertek Testing Services NA, Inc. dba Intertek Building & Construction (B&C) was contracted by Johnson Gas Appliance Company, 1155 Sherman Road, Hiawatha, IA 52233 to perform testing in accordance with EPA 40 CFR Part 60, "Standards of Performance for New Residential Wood Heaters, New Residential Hydronic Heaters and Forced-Air Furnaces," ASTM E2515-2017, "Standard Test Method for Determination of Particulate Matter Emissions Collected by a Dilution Tunnel," ASTM E2779-2017, "Standard Test Method for Determining Particulate Matter Emissions from Pellet Heaters," and CSA B415.1-2010 (R2020), "Performance Testing of Solid-Fuel-Burning Heating Appliances" on their model Element-P II Pellet Fuel Room Heater. Results obtained are tested values and were secured by using the designated test method(s). Testing was conducted at Intertek test facility in Middleton, WI.

Unless differently required, Intertek reports apply the "Simple Acceptance" rule also called "Shared Risk approach," of ILAC-G8:09/2019, Guidelines on Decision Rules and Statements of Conformity.

Intertek B&C will service this report for the entire test record retention period. The test record retention period ends four years after the test date. Test records, such as detailed drawings, datasheets, representative samples of test specimens (where required by Certification or Accreditation bodies), or other pertinent project documentation, will be retained for the entire test record retention period.

For INTERTEK B&C:

|                      |                                                                                                   |
|----------------------|---------------------------------------------------------------------------------------------------|
| <b>COMPLETED BY:</b> | Ken Slater                                                                                        |
| <b>TITLE:</b>        | Associate Engineer –<br>Hearth                                                                    |
| <b>SIGNATURE:</b>    | <br>Ken Slater |
| <b>DATE:</b>         | 11/09/23                                                                                          |

|                     |                                                                                       |
|---------------------|---------------------------------------------------------------------------------------|
| <b>REVIEWED BY:</b> | Brian Ziegler                                                                         |
| <b>TITLE:</b>       | Technical Team Leader-<br>Hearth                                                      |
| <b>SIGNATURE:</b>   |  |
| <b>DATE:</b>        | 11/09/23                                                                              |

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**TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY**

Report No.: 105164443MID-005R2

Date: 11/09/23

**SECTION 2****SUMMARY OF TEST RESULTS**

The appliance tests resulted in the following performance:

Particulate Emissions: 1.05 g/hr

Carbon Monoxide Emissions: 0.0047 g/min

Heating Efficiency: 78.5% (Higher Heating Value Basis)

**SECTION 3****TEST METHOD(S)**

The specimen was evaluated in accordance with the following:

**EPA 40 CFR Part 60-2015**, *Standards of Performance for New Residential Wood Heaters, New Residential Hydronic Heaters and Forced-Air Furnaces*

**ASTM E2515-2017**, *Standard Test Method for Determination of Particulate Matter Emissions Collected by a Dilution Tunnel*

**ASTM E2779-2017**, *Standard Test Method for Determining Particulate Matter Emissions from Pellet Heaters*

**CSA B415.1-2010 (R2020)**, *Performance Testing of Solid-Fuel-Burning Heating Appliances*

**SECTION 4****MATERIAL SOURCE/INSTALLATION**

A sample was submitted to Intertek directly from the client. The sample was not independently selected for testing. The test unit was received at Intertek in Middleton, WI on 10/24/22 and was shipped via the client. The unit was inspected upon receipt and found to be in good condition. The unit was set up following the manufacturer's instructions without difficulty.

Following assembly, the unit was placed on the test stand. Prior to beginning the emissions tests, Johnson Gas Appliance Company staff operated the unit for a minimum of 48 hours at a medium burn rate to break in the stove. The unit was found to be operating satisfactory during this break-in. The 48 plus hours of pre-burning were conducted from 8/22/22 to 8/29/22. The fuel used for the break-in process was wood pellets.

Following the pre-burn break-in process the unit was allowed to cool and ash and residue was removed from the firebox. The unit's chimney system and laboratory dilution tunnels were cleaned using standard wire brush chimney cleaning equipment. On 10/26/22 the unit was set-up for testing.

## TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY

Report No.: 105164443MID-005R2

Date: 11/09/23

### SECTION 5

#### EQUIPMENT

| EQUIPMENT           | INV NUMBER | CALIBRATION DUE | MU                   |
|---------------------|------------|-----------------|----------------------|
| Timer               | 646        | 4/5/23          | 0.06 sec             |
| Timer               | 1213       | 4/5/23          | 0.06 sec             |
| Pressure Transducer | 1406       | 1/13/23         | 0.00006 (inH2O)      |
| Data Acquisition    | 986        | 4/0/23          | 0.06 °F              |
| Platform Scale      | 1134       | 4/01/23         | .118 lbs             |
| Hygrometer          | 1450       | 2/16/23         | .033 inH2O; 0.35 %RH |
| Flow Meter          | 1413       | 3/20/23         | 0.0075 slpm          |
| Flow Meter          | 1414       | 3/20/23         | 0.0075 slpm          |
| Flow Meter          | 1519       | 3/20/23         | 0.0074 slpm          |
| Balance             | 713        | 4/04/23         | 0.00007 g            |
| Anemometers         | 1457       | 4/04/23         | 5 fpm                |
| Mercurial Barometer | 437        | NA              | 0.05 in              |

### SECTION 6

#### LIST OF OFFICIAL OBSERVERS

| NAME          | COMPANY                       |
|---------------|-------------------------------|
| Ken Slater    | Intertek B&C                  |
| Terry Krumrei | Johnson Gas Appliance Company |

### SECTION 7

#### TEST PROCEDURE

On 10/26/22, the unit was tested for EPA emissions. For pellet stoves, the test was conducted in accordance with ASTM E2779. The fuel used for the test run was premium-Grade Pellets (Marthwood).

The applicable EPA regulatory limits are:

Step 1 – 2015 – 4.5 grams per hour.

Step 2 – 2020 – 2.0 grams per hour.

**TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY**

Report No.: 105164443MID-005R2

Date: 11/09/23

**TEST SET-UP DESCRIPTION**

A 3" vertical flue is connected by adapters to a standard 6" diameter vertical single wall pipe and insulated chimney system was installed to 15' above floor level. The single wall pipe extended to 8 feet above the floor and insulated chimney extended the remaining height.

**AIR SUPPLY SYSTEM**

Combustion air enters a 2" inlet pipe located on the back of the heater, which is directed to the pellet burn pot. All gases exit through the 3" flue also located at the back of the heater. The exhaust gases are assisted by a combustion blower.

**TEST FUEL PROPERTIES**

Wood pellets used for the testing were Marth premium grade hardwood pellets, with a majority of the wood species consisting of oak and maple. The pellets have a measured heating value of 7968 Btu/hr (kJ/kg 18533) and a moisture content of 3.70% on a dry basis and 3.57% on a wet basis.

**SAMPLING LOCATIONS**

Particulate samples are collected from the dilution tunnel at a point 20 feet from the tunnel entrance. The tunnel has two elbows in the system ahead of the sampling section. (See Figure 3.) The sampling section is a continuous 13-foot section of 6 inch diameter pipe straight over its entire length. Tunnel velocity pressure is determined by a standard Pitot tube located 60 inches from the beginning of the sampling section. The dry bulb thermocouple is located six inches downstream from the Pitot tube. Tunnel samplers are located 60 inches downstream of the Pitot tube and 36 inches upstream from the end of this section. (See Figure 1.)

Stack gas samples are collected from the steel chimney section 8 feet  $\pm$  6 inches above the scale platform. (See Figure 2.)

# TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY

Report No.: 105164443MID-005R2

Date: 11/09/23

**FIGURE 1 – DILUTION TUNNEL**

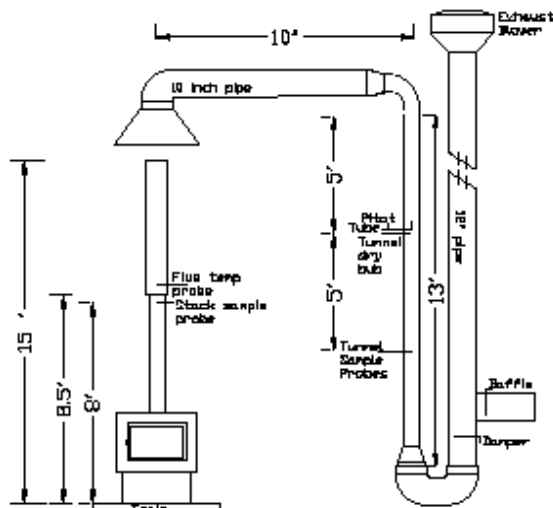
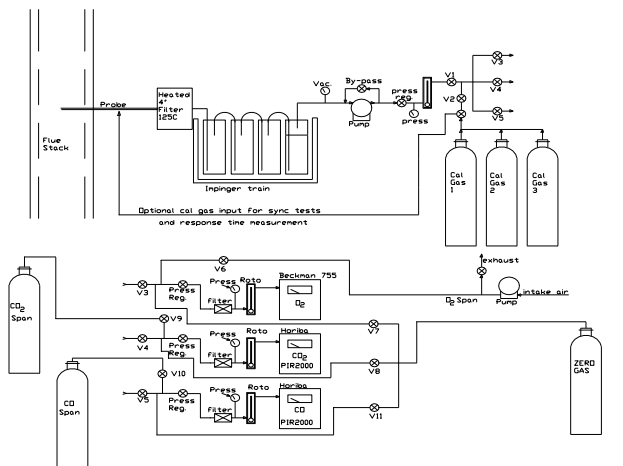


FIGURE 1

**FIGURE 2 – STACK GAS SAMPLE TRAIN**



ITS FLUE GAS SAMPLE TRAIN

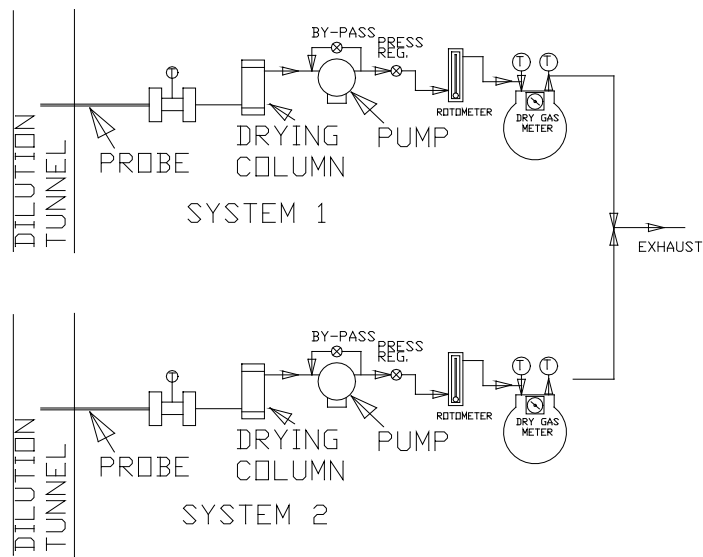
FIGURE 2

## TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY

Report No.: 105164443MID-005R2

Date: 11/09/23

### FIGURE 3 – DILUTION TUNNEL SAMPLE SYSTEMS



**Figure 3**

## SAMPLING METHODS

### PARTICULATE SAMPLING

Particulates were sampled in strict accordance with ASTM E2515. This method uses two identical sampling systems with Merck Millipore AP4004700 Glass Fibre, 47-mm diameter filters. The dryers used in the sample systems are filled with “Drierite” before each test run. In order to measure first-hour emissions rates a third filter sample train is prepared separate of the required two train system for the total emissions rate. The filter set are analyzed individually to determine the first hour and total emissions rate.

## INSTRUMENT CALIBRATION

### DRY GAS METERS

At the conclusion of each test program the dry gas meters are checked against our standard dry gas meter. Three runs are made on each dry gas meter used during the test program. The average calibration factors obtained are then compared with the six-month calibration factor and, if within

**TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY**

Report No.: 105164443MID-005R2

Date: 11/09/23

5%, the six-month factor is used to calculate standard volumes. Results of this calibration are contained in Appendix D.

An integral part of the post-test calibration procedure is a leak check of the pressure side by plugging the system exhaust and pressurizing the system to 10" W.C. The system is judged to be leak free if it retains the pressure for at least 10 minutes.

The standard dry gas meter is calibrated every 6 months using a Spirometer designed by the EPA Emissions Measurement Branch. The process involves sampling the train operation for 1 cubic foot of volume. With readings made to .001 ft<sup>3</sup>, the resolution is .1%, giving an accuracy higher than the  $\pm 2\%$  required by the standard.

**STACK SAMPLE ROTAMETER**

The stack sample rotometer is checked by running three tests at each flow rate used during the test program. The flow rate is checked by running the rotometer in series with one of the dry gas meters for 10 minutes with the rotometer at a constant setting. The dry gas meter volume measured is then corrected to standard temperature and pressure conditions. The flow rate determined is then used to calculate actual sampled volumes.

**GAS ANALYZERS**

The continuous analyzers are zeroed and spanned before each test with appropriate gases. A mid-scale multi-component calibration gas is then analyzed (values are recorded). At the conclusion of a test, the instruments are checked again with zero, span and calibration gases (values are recorded only). The drift in each meter is then calculated and must not exceed 5% of the scale used for the test.

At the conclusion of each unit test program, a three-point calibration check is made. This calibration check must meet accuracy requirements of the applicable standards. Consistent deviations between analyzer readings and calibration gas concentrations are used to correct data before computer processing. Data is also corrected for interferences as prescribed by the instrument manufacturer's instructions.

**TEST METHOD PROCEDURES****LEAK CHECK PROCEDURES**

Before and after each test, each sample train is tested for leaks. Leakage rates are measured and must not exceed 0.02 CFM or 4% of the sampling rate. Leak checks are performed checking the entire sampling train, not just the dry gas meters. Pre-test and post-test leak checks are conducted with a vacuum of 10 inches of mercury. Vacuum is monitored during each test and the highest vacuum reached is then used for the post-test vacuum value. If leakage limits are not

## TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY

Report No.: 105164443MID-005R2

Date: 11/09/23

met, the test run is rejected. During, these tests the vacuum was typically less than 2 inches of mercury. Thus, leakage rates reported are expected to be much higher than actual leakage during the tests.

### TUNNEL VELOCITY/FLOW MEASUREMENT

The tunnel velocity is calculated from a center point Pitot tube signal multiplied by an adjustment factor. This factor is determined by a traverse of the tunnel as prescribed in EPA Method 1. Final tunnel velocities and flow rates are calculated from EPA Method 2, Equation 6.9 and 6.10. (Tunnel cross sectional area is the average from both lines of traverse.)

Pitot tubes are cleaned before each test and leak checks are conducted after each test.

### PM SAMPLING PROPORTIONALITY

Proportionality was calculated in accordance with ASTM E2515-2017. The data and results are included in Appendix C.

### DEVIATIONS FROM STANDARD METHOD:

None

## SECTION 8

### TEST CALCULATIONS

#### WEIGHT OF TEST FUEL BURNED (DRY) – ASTM E2779

$$M_{Bdb} = (M_{Swb} - M_{Ewb})(100/(100 + FM))$$

where:

FM = average fuel moisture of test fuel, % dry basis,

$M_{Swb}$  = weight of test fuel in hopper at start of test run, wet basis, kg (lb),

$M_{Ewb}$  = weight of test fuel in hopper at end of test run, wet basis, kg (lb), and

$M_{Bdb}$  = weight of test fuel burned during test run, dry basis, kg (lb).

#### WEIGHT OF TEST FUEL BURNED PER TEST SEGMENT (DRY) – ASTM E2779

$$M_{BSidb} = (M_{SSiwb} - M_{ESiwb})(100/(100 + FM))$$

where:

$M_{SSiwb}$  = weight of test fuel in hopper at start of test run segment  $i$ , wet basis, kg (lb),

$M_{ESiwb}$  = weight of test fuel in hopper at end of test run segment  $i$ , wet basis, kg (lb),

$M_{BSidb}$  = weight of test fuel burned during test run segment  $i$ , dry basis, kg (lb), and

$i$  = test run segments in accordance with 9.4, Table 1.

## TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY

Report No.: 105164443MID-005R2

Date: 11/09/23

### AVERAGE BURN RATE FOR FULL TEST (DRY) – ASTM E2779

$$BR = 60 M_{Bdb} / \theta$$

where:

BR = average dry burn rate over the full integrated test run, kg/h (lb/h), and

$\theta$  = total length of full integrated test run, min.

### AVERAGE BURN RATE PER TEST SEGMENT (DRY) – ASTM E2779

$$BR_{Si} = 60 M_{BSdb} / \theta_{Si}$$

where:

$BR_{Si}$  = average dry burn rate over test run segment  $i$ , kg/h (lb/h), and

$\theta_{Si}$  = total length of test run segment  $i$ , min.

### AVERAGE EMISSION RATE FOR FULL TEST (g/hr) – ASTM E2779

$$PM_R = 60(E_T / \theta)$$

where:

$E_T$  = total particulate emissions for full integrated test run measured using Test Method E2515, g (lb),

$\theta$  = total length of test run, min, and

$PM_R$  = average particulate emission rate over the full integrated test run, g/h.

### AVERAGE EMISSION FACTOR FOR FULL TEST (g/kg dry) – ASTM E2779

$$PM_F = E_T / M_{Bdb}$$

where:

$PM_F$  = average particulate emission factor over the full integrated test run, g/dry kg of fuel burned.

### AVERAGE EMISSIONS FOR FULL TEST (g/MJ or lb/MMBtu) – ASTM E2779

$$PM_H = E_T / E_O$$

where:

$E_O$  = average measured overall heat output over the full integrated test run from [Annex A1](#), MJ (MMBTU), and

$PM_H$  = average particulate emissions in accordance with unit of average heat output over the full integrated test run, g/MJ (lb/MMBtu).

### NOMENCLATURE FOR ASTM E2515:

A = Cross-sectional area of tunnel m<sup>2</sup> (ft<sup>2</sup>).

## TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY

Report No.: 105164443MID-005R2

Date: 11/09/23

- $B_{ws}$  = Water vapor in the gas stream, proportion by volume (assumed to be 0.02 (2.0 %)).
- $C_p$  = Pitot tube coefficient, dimensionless (assigned a value of 0.99).
- $C_r$  = Concentration of particulate matter room air, dry basis, corrected to standard conditions, g/dscm (gr/dscf) (mg/dscf).
- $C_s$  = Concentration of particulate matter in tunnel gas, dry basis, corrected to standard conditions, g/dscm (gr/dscf) (mg/dscf).
- $E_T$  = Total particulate emissions, g.
- $F_p$  = Adjustment factor for center of tunnel pitot tube placement.  
 $F_p = V_{strav}/V_{scent}$
- $K_p$  = Pitot Tube Constant,  $34.97 \frac{m}{sec} \left[ \frac{(\frac{g}{g} \text{ mole})(mm Hg)}{(K)(mm water)} \right]^{\frac{1}{2}}$   
 or  
 = Pitot Tube Constant,  $85.49 \frac{ft}{sec} \left[ \frac{(\frac{lb}{lb} \text{ mole})(in Hg)}{(R)(in water)} \right]^{\frac{1}{2}}$
- $L_a$  = Maximum acceptable leakage rate for either a pretest or post-test leak-check, equal to 0.0003 m<sup>3</sup>/min (0.010 cfm) or 4 % of the average sampling rate, whichever is less.
- $L_p$  = Leakage rate observed during the post-test leak-check, m<sup>3</sup>/min (cfm).
- $m_p$  = mass of particulate from probe, mg.
- $m_f$  = mass of particulate from filters, mg.
- $m_g$  = mass of particulate from filter gaskets, mg.
- $m_r$  = mass of particulate from the filter, filter gasket, and probe assembly from the room air blank filter holder assembly, mg.
- $m_n$  = Total amount of particulate matter collected, mg.
- $M_s$  = the dilution tunnel dry gas molecular weight (may be assumed to be 29 g/g mole (lb/lb mole)).
- $P_{bar}$  = Barometric pressure at the sampling site, mm Hg (in. Hg).
- $P_g$  = Static Pressure in the tunnel (in. water).
- $P_R$  = Percent of proportional sampling rate.
- $P_s$  = Absolute average gas static pressure in dilution tunnel, mm Hg (in. Hg).
- $P_{std}$  = Standard absolute pressure, 760 mm Hg (29.92 in. Hg).
- $Q_{std}$  = Average gas flow rate in dilution tunnel.  
 $Q_{std} = 60 (1 - B_{ws}) V_s A [T_{std} P_s / T_s P_{std}]$   
 dscm/min (dscf/min).
- $T_m$  = Absolute average dry gas meter temperature, K (R).
- $T_{mi}$  = Absolute average dry gas meter temperature during each 10-min interval,  $i$ , of the test run.

$$T_{mi} = (T_{mi(b)} + T_{mi(e)})/2$$

where:

- $T_{mi(b)}$  = Absolute dry gas meter temperature at the beginning of each 10-min test interval,  $i$ , of the test run, K (R), and
- $T_{mi(e)}$  = Absolute dry gas meter temperature at the end of each 10-min test interval,  $i$ , of the test run, K (R).

## TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY

Report No.: 105164443MID-005R2

Date: 11/09/23

$T_s$  = Absolute average gas temperature in the dilution tunnel, K (R).

$T_{si}$  = Absolute average gas temperature in the dilution tunnel during each 10-min interval,  $i$ , of the test run, K (R).

$$T_{si} = (T_{si(b)} + T_{m=si(e)})/2$$

where:

$T_{si(b)}$  = Absolute gas temperature in the dilution tunnel at the beginning of each 10-min test interval,  $i$ , of the test run, K (R), and

$T_{si(e)}$  = Absolute gas temperature in the dilution tunnel at the end of each 10-min test interval,  $i$ , of the test run, K (R).

$V_m$  = Volume of gas sample as measured by dry gas meter, dcm (dcf).

$V_{mc}$  = Volume of gas sampled corrected for the post test leak rate, dcm (dcf).

$V_{mi}$  = Volume of gas sample as measured by dry gas meter during each 10-min interval,  $i$ , of the test run, dcm.

$V_{m(std)}$  = Volume of gas sample measured by the dry gas meter, corrected to standard conditions.

$$V_{m(std)} = K_1 V_m Y [(P_{bar} + (\Delta H/13.6))/T_m]$$

where:

$K_1$  = 0.3855 K/mm Hg for SI units and = 17.64 R/in. Hg for inch-pound units.

$$V_{m(std)} = K_1 V_{mc} Y [(P_{bar} + (\Delta H/13.6))/T_m]$$

where:

$V_{mc}$  =  $V_m - (L_p - L_a)u$

$V_{mr}$  = Volume of room air sample as measured by dry gas meter, dcm (dcf), and

$V_{mr(std)}$  = Volume of room air sample measured by the dry gas meter, corrected to standard conditions.

$$V_{mr(std)} = K_1 V_{mr} Y [(P_{bar} + (\Delta H/13.6))/T_m]$$

Where:

$K_1$  = 0.3855 K/mm Hg for SI units and = 17.64 R/in. Hg for inch-pound units, and

$V_s$  = Average gas velocity in the dilution tunnel.

$$V_s = F_p K_p C_p (V \Delta P_{avg}) (V(T_s/P_s M_s))$$

$V_{si}$  = Average gas velocity in dilution tunnel during each 10-min interval,  $i$ , of the test run.

$$V_{si} = F_p K_p C_p (V \Delta P_i) (V(T_{si}/P_s M_s))$$

$V_{scent}$  = Average gas velocity at the center of the dilution tunnel calculated after the Pitot tube traverse.

$V_{strav}$  = Average gas velocity calculated after the multipoint Pitot traverse.

$Y$  = Dry gas meter calibration factor.

$\Delta H$  = Average pressure at the outlet of the dry gas meter or the average differential pressure across the orifice meter, if used, mm water (in. water).

$\Delta P_{avg}$  = Average velocity pressure in the dilution tunnel, mm water (in. water).

$\Delta P_i$  = Velocity pressure in the dilution tunnel as measured with the Pitot tube during each 10-min interval,  $i$ , of the test run.

$$\Delta P_i = (\Delta P_{i(b)} + \Delta P_{i(e)})/2$$

## TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY

Report No.: 105164443MID-005R2

Date: 11/09/23

where:

- $\Delta P_{i(b)}$  = Velocity pressure in the dilution tunnel as measured with the Pitot tube at the beginning of each 10-min interval, i, of the test run, mm water (in. water), and
- $\Delta P_{i(e)}$  = Velocity pressure in the dilution tunnel as measured with the Pitot tube at the end of each 10-min interval, i, of the test run, mm water (in. water).
- $\theta$  = Total sampling time, min.
- 10 = ten min, length of first sampling period.
- 13.6 = Specific gravity of mercury.
- 100 = Conversion to percent.

### TOTAL PARTICULATE WEIGHT – ASTM E2515

$$M_n = m_p + m_f + m_g$$

### PARTICULATE CONCENTRATION – ASTM E2515

$$C_s = K_2(m_n/V_{m(std)}) \text{ g/dscm (g/dscf)}$$

where:

$$K_2 = 0.001 \text{ g/mg}$$

### TOTAL PARTICULATE EMISSIONS (g) – ASTM E2515

$$E_T = (C_s - C_r)Q_{std}\theta$$

### PROPORTIONAL RATE VARIATION (%) – ASTM E2515

$$PR = [\theta(V_{mi} V_s T_m T_{si}) / (10(V_m V_{si} T_s T_{mi}))] \times 100$$

### MEASUREMENT OF UNCERTAINTY – ASTM E2515

$$MU_{\text{weighing}} = \sqrt{0.1^2} \cdot X$$

### GENERAL FORMULA – ASTM E2515

$$uY = \sqrt{((\delta Y / \delta x_1) \times u_1)^2 + \dots + ((\delta Y / \delta x_n) \times u_n)^2}$$

Where:

$\delta Y / \delta x_i$  = Partial derivative of the combining formula with respect to individual measurement xi,

$u_i$  = is the uncertainty associated with that measurement.

### TOTAL PARTICULATE EMISSIONS – ASTM E2515

$$E_T = (C_s - C_r) Q_{std} \theta$$

where:

$C_s$  = sample filter catch/(sample flow rate x test duration), g/dscf,

$C_r$  = room background filter catch/(sample flow x sampling time), g/dscf,

$Q_{std}$  = average dilution tunnel flow rate, dscf/min, and

$\theta$  = sampling time, minutes.

### MU OF $C_s$

$$C_s = F_c / (Q_{\text{sample}} \times \theta) = 0.025 / (0.25 \times 180) = 0.0005555$$

## TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY

Report No.: 105164443MID-005R2

Date: 11/09/23

$$\begin{aligned}\delta c_s / \delta F_c &= 1 / Q_{\text{sample}} \cdot \Theta = 1 / 0.25 \cdot 180 = 0.0222 \\ \delta c_s / \delta Q_{\text{sample}} &= -F_c / Q_{\text{sample}}^2 \cdot \Theta = -0.025 / 0.25^2 \cdot 180 = -0.00222 \\ \delta c_s / \delta \Theta &= -F_c / Q_{\text{sample}} \cdot \Theta^2 = -0.025 / 0.25 \cdot 180^2 = -0.000003 \\ \text{MU}_{c_s} &= \sqrt{(0.00027 \cdot 0.0222)^2 + (0.0025 \cdot -0.00222)^2} \\ &\quad \sqrt{+ (0.1 \cdot -0.000003)^2} = 0.0000091\text{g} \\ \text{Thus, } c_s &\text{ would be } 0.555 \text{ mg/dscf} \pm 0.0081 \text{ mg/dscf at 95\% confidence level.}\end{aligned}$$

### MU OF $c_r$

$$\begin{aligned}c_r &= BG_c / (Q_{BG} \times \Theta) = 0.002 / (0.15 \times 180) = 0.000074 \\ \delta c_r / \delta BG_c &= 1 / Q_{BG} \cdot \Theta = 1 / 0.15 \cdot 180 = 0.03704 \\ \delta c_r / \delta Q_{BG} &= -BG_c / Q_{BG}^2 \cdot \Theta = -0.002 / 0.15^2 \cdot 180 = -0.0004938 \\ \delta c_r / \delta \Theta &= -BG_c / Q_{BG} \cdot \Theta^2 = -0.002 / 0.15 \cdot 180^2 = -0.0000004 \\ \text{MU}_{c_r} &= \sqrt{(0.00027 \cdot 0.03704)^2 + (0.0015 \cdot -0.0004938)^2} \\ &\quad \sqrt{+ (0.1 \cdot -0.0000004)^2} = 0.00001\text{g} \\ \text{Thus, } c_r &\text{ would be } 0.074 \text{ mg/dscf} \pm 0.01 \text{ mg/dscf at 95\% confidence level.}\end{aligned}$$

### $E_T$ AND $\text{MU}_{E_T}$

$$\begin{aligned}E_T &= (c_s - c_r) Q_{\text{std}} \Theta = (0.000555 - 0.000074) \times 150 \times 180 = 13.00\text{g} \\ \delta E_T / \delta c_s &= Q_{\text{std}} \cdot \Theta = 150 \cdot 180 = 27,000 \\ \delta E_T / \delta c_r &= Q_{\text{std}} \cdot \Theta = 150 \cdot 180 = 27,000 \\ \delta E_T / \delta Q_{\text{std}} &= c_s \cdot \Theta - c_r \cdot \Theta = 0.000555 \cdot 180 - 0.000074 \cdot 180 = 0.08667 \\ \delta E_T / \delta \Theta &= c_s \cdot Q_{\text{std}} - c_r \cdot Q_{\text{std}} = 0.000555 \cdot 180 - 0.000074 \cdot 180 = 0.07222 \\ \text{MU}_{E_T} &= \sqrt{(27,000 \cdot 0.0000081)^2 + (27,000 \cdot 0.00001)^2 (0.08667 \cdot 3)^2} \\ &\quad \sqrt{+ (0.07222 \cdot 0.1)^2} = 0.436\end{aligned}$$

Thus the result in this example would be:  
 $E_T = 13.00\text{g} \pm 0.44 \text{ g}$  at a 95% confidence level.

### EFFICIENCY – CSA B415.1

The change in enthalpy of the circulating air shall be calculated using the moisture content and temperature rise of the circulating air, as follows:

$$\Delta h = \Delta t (1.006 + 1.84x)$$

Where:

$\Delta h$  = change in enthalpy, kJ/kg  
 $\Delta t$  = temperature rise, °C  
1.006 = specific heat of air, kJ/kg °C  
1.84 = specific heat of water vapor, kJ/kg °C  
 $x$  = humidity ratio, kg/kg

## TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY

Report No.: 105164443MID-005R2

Date: 11/09/23

The equivalent duct diameter shall be calculated as follows:

$$ED = 2HW/H+W$$

Where:

ED = equivalent duct diameter

H = duct height, m

W = duct width, m

The air flow velocity shall be calculated as follows:

$$V = F_p \times C_p \times 34.97 \times \sqrt{T/28.56(P_{\text{baro}} + P_s)}$$

where

V = velocity, m/s

F<sub>p</sub> = Pitot tube calibration factor determined from vane anemometer measurements

C<sub>p</sub> = Pitot factor

= 0.99 for a standard Pitot tube or as determined by calibration for a Type S Pitot tube

34.97 = Pitot tube constant

**Note:** The Pitot tube constant is determined on the basis of the following units:

m/s[g/g mole (mm Hg)/(K)(mm H<sub>2</sub>O)]<sup>0.5</sup>

ΔP = velocity pressure, mm H<sub>2</sub>O

T = temperature, K

28.56 = molecular weight of air

P<sub>Baro</sub> = barometric pressure, mm Hg

P<sub>s</sub> = duct static pressure, mm Hg

The mass flow rate shall be calculated as follows:

$$m = 3600VAp$$

where:

m = mass flow rate, kg/h

V = air flow velocity, m/s

3600 = number of seconds per hour

A = duct cross-sectional area, m<sup>2</sup>

p = density of air at standard temperature and pressure (use 1.204 kg/m<sup>3</sup>)

The rate of heat release into the circulating air shall be calculated using the air flow and change in enthalpy, as follows:

$$\Delta e = \Delta h \times m$$

## TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY

Report No.: 105164443MID-005R2

Date: 11/09/23

Where:

$\Delta e$  = rate of heat release into the circulating air, kJ/h

$\Delta h$  = change in enthalpy of the circulating air, kJ/kg

$m$  = mass air flow rate, kg/h

The heat output over any time interval shall be calculated as the sum of the heat released over each measurement time interval, as follows:

$$E_t = \sum(\Delta e \times i) \text{ for } i = t_1 \text{ to } t_2$$

Where:

$E_t$  = delivered heat output over any time interval  $t_2 - t_1$ , kJ

$i$  = time interval for each measurement, h

The average heat output rate over any time interval shall be calculated as follows:

$$e_t = E_t / t$$

where

$e_t$  = average heat output, kJ/h

$t$  = time interval over which the average output is desired, h

The total heat output during the burn shall be calculated as the sum of all the heat outputs over each time interval, as follows:

$$E_d = \sum(E_t) \text{ for } t = t_0 \text{ to } t_{\text{final}}$$

Where:

$E_d$  = heat output over a burn, kJ/h (Btu/h)

$E_t$  = heat output during each time interval, kJ/h (Btu/h)

The efficiency shall be calculated as the total heat output divided by the total energy input, expressed as a percentage as follows:

$$\text{Efficiency, \%} = 100 \times E_d / I$$

Where:

$E_d$  = total heat output of the appliance over the test period, kJ/kg

$I$  = input energy (fuel calorific value as-fired times weight of fuel charge), kJ/kg (Btu/lb)

## TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY

Report No.: 105164443MID-005R2

Date: 11/09/23

### SECTION 9

#### TEST SPECIMEN DESCRIPTION

The model Element-P II Pellet Fuel Room Heater is constructed of sheet steel. The outer dimensions are 21.5-inches/546mm deep, 31-inches/787mm high, and 20.5-inches/521mm wide. The heat exchanger is located directly above the firebox with outlet air grille positioned above the firebox access door. A galvanized steel fuel hopper located at the top back of the unit.

### SECTION 10

#### TEST RESULTS

##### DESCRIPTION OF TEST RUNS:

RUN #1 (10/26/22): The test for pellet heaters is a continuous test with three separate burn rates. At 8:42 am the unit was started and operated for a minimum of 1 hour for the pretest operation. At 9:42 am the unit was set to the maximum feed rate (level 5) with a burn rate of 2.36 kg/hr (wet), the scale was tared and a 25-lb weight was added to the scale to determine feed rate of the fuel, and the sampling system was started. At 10:42 am, the system #3 sampling filter was changed out and the unit was set to ≤50% feed rate (level 2) with a burn rate of 1.07 kg/hr (wet). At 12:42 pm, the heater was changed to the minimum feed rate (level 1) with a burn rate of 0.73 kg/hr (wet). At 3:42 pm, testing was completed. The total burn time was 360 minutes.

The test run has been found to be appropriate, with no anomalies, and the test run has been validated and is deemed compliant. No negative weight was found on the filters, as the filters and gaskets are weighed together to eliminate filter material transfer to gaskets. All weightings were handled properly, with no negative weight on gaskets or probes.

**TABLE 1 – EMISSIONS**

| RUN # | TEST DATE | BURN RATES (kg/hr)(wet) |      | PARTICULATE EMISSION RATE (g/hr) | 1 <sup>st</sup> HOUR EMISSIONS (g) | CO EMISSIONS (g/min) | HEATING EFFICIENCY (%HHV) |
|-------|-----------|-------------------------|------|----------------------------------|------------------------------------|----------------------|---------------------------|
| 1     | 10/26/22  | H*                      | 2.36 | 1.05                             | 1.54                               | 0.0047               | 78.5%                     |
|       |           | M*                      | 1.07 |                                  |                                    |                      |                           |
|       |           | L*                      | 0.73 |                                  |                                    |                      |                           |
|       |           | OA*                     | 1.11 |                                  |                                    |                      |                           |

\*Notes: H= High burn rate, M= Medium burn rate, L= low burn rate, OA= overall burn rate.

**TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY**

Report No.: 105164443MID-005R2

Date: 11/09/23

**TABLE 2 – TEST FACILITY CONDITIONS**

| RUN # | ROOM TEMP BEFORE (°F) | ROOM TEMP AFTER (°F) | BARO PRES BEFORE (in/Hg) | BARO PRES AFTER (in/Hg) | R. H. BEFORE (%) | R. H. AFTER (%) | AIR VEL BEFORE (ft/min) | AIR VEL AFTER (ft/min) |
|-------|-----------------------|----------------------|--------------------------|-------------------------|------------------|-----------------|-------------------------|------------------------|
| 1     | 70                    | 70                   | 29.03                    | 29.04                   | 30.9             | 28.9            | 0                       | 0                      |

**TABLE 3 – DILUTION TUNNEL FLOW RATE MEASUREMENTS AND SAMPLING DATA**

| RUN # | BURN TIME (min) | VELOCITY (ft/sec) | VOLUMETRIC FLOW RATE (dscf/min) | AVG TEMP (°R) | SAMPLE VOLUME (dscf) |       | PARTICULATE CATCH (mg) |      |
|-------|-----------------|-------------------|---------------------------------|---------------|----------------------|-------|------------------------|------|
|       |                 |                   |                                 |               | 1                    | 2     | 1                      | 2    |
| 1     | 360             | 21.30             | 231.76                          | 543.39        | 48.56                | 49.43 | 3.80                   | 3.60 |

**TABLE 4 - DILUTION TUNNEL DUAL TRAIN PRECISION**

| RUN # | SAMPLE RATIOS |         | TOTAL EMISSIONS (g) |         | DEVIATION (%) | DEVIATION (g/kg) |
|-------|---------------|---------|---------------------|---------|---------------|------------------|
|       | TRAIN 1       | TRAIN 2 | TRAIN 1             | TRAIN 2 |               |                  |
| 1     | 1718.20       | 1687.91 | 6.53                | 6.08    | 3.59          | 0.068            |

**TABLE 5 - GENERAL SUMMARY OF RESULTS**

| RUN # | BURN RATE (kg/hr)(dry) (OVERALL) | INITIAL DRAFT (in/H <sub>2</sub> O) | RUN TIME (min) | AVERAGE DRAFT (in/H <sub>2</sub> O) |
|-------|----------------------------------|-------------------------------------|----------------|-------------------------------------|
| 1     | 1.11                             | 0.028                               | 360            | 0.023                               |

**TABLE 6 - CSA B415.1 RESULTS**

| BURN RATE (kg/hr)(dry) | CO EMISSIONS (g/min) | HEATING EFFICIENCY (% HHV) | HEAT OUTPUT (Btu/hr) |
|------------------------|----------------------|----------------------------|----------------------|
| HIGH – 2.28            | 0.0074               | 79.4                       | 31,773               |
| MEDIUM – 1.03          | 0.0046               | 77.7                       | 14,073               |
| LOW – 0.70             | 0.0041               | 75.5                       | 9,318                |
| OVERALL – 1.07         | 0.0047               | 78.5                       | 14,820               |



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## TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY

Report No.: 105164443MID-005R2

Date: 11/09/23

### SECTION 11

#### CONCLUSION

This test demonstrates that this unit is an affected facility under the definition given in the regulation. The emission rate of 1.05 g/hr meets the EPA requirements for the Step 2 limits.

## TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY

Report No.: 105164443MID-005R2

Date: 11/09/23

### SECTION 12

#### PHOTOGRAPHS

**Photo No. 1**  
**Emissions Test # 1**



**TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY**

Report No.: 105164443MID-005R2

Date: 11/09/23

**Photo No. 2**  
**Security Label Front side**



## TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY

Report No.: 105164443MID-005R2

Date: 11/09/23

**Photo No. 3**  
**Security Label Back Side**

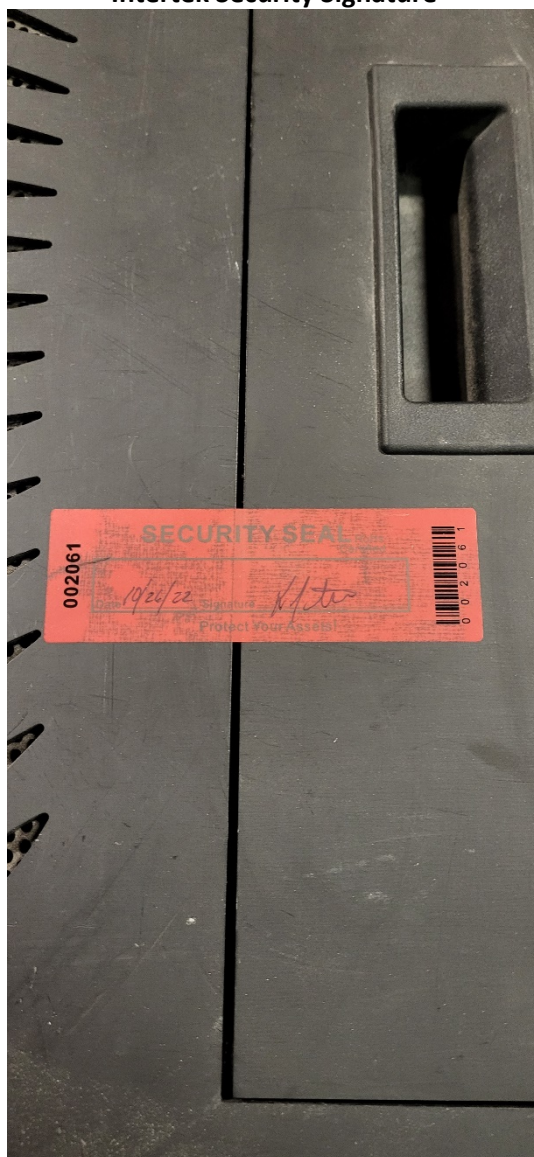


## TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY

Report No.: 105164443MID-005R2

Date: 11/09/23

Photo No. 4  
Intertek Security Signature

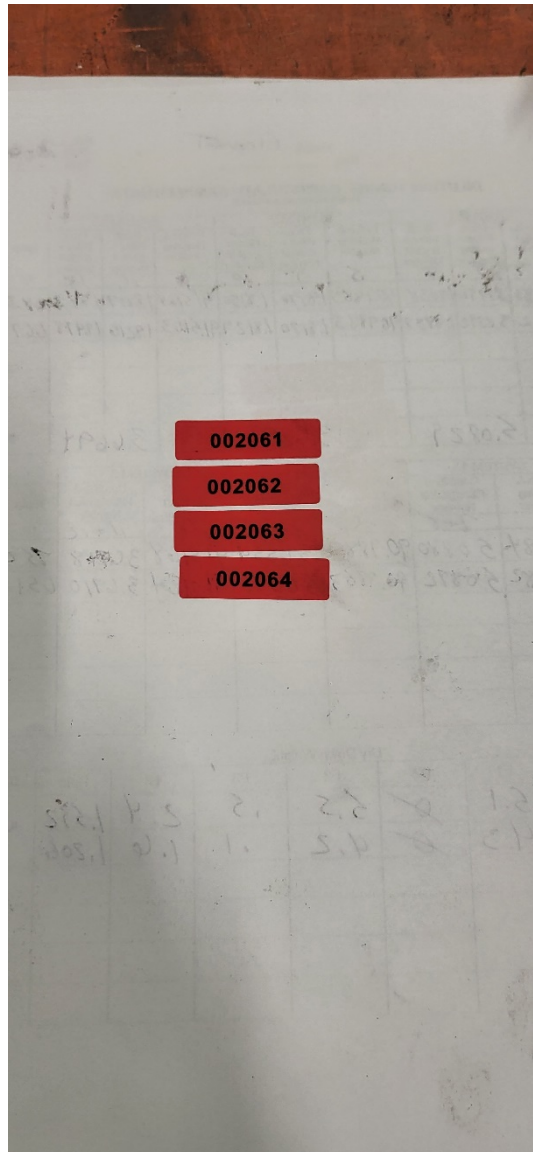


**TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY**

Report No.: 105164443MID-005R2

Date: 11/09/23

**Photo No. 5**  
**Security Label Numbers**



**TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY**

Report No.: 105164443MID-005R2

Date: 11/09/23

**Photo No. 6**  
**Wrapped Unit**





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## TEST REPORT FOR JOHNSON GAS APPLIANCE COMPANY

Report No.: 105164443MID-005R2

Date: 11/09/23

### SECTION 13

#### REVISION LOG

| REVISION # | DATE     | SECTION    | REVISION                                                                                          |
|------------|----------|------------|---------------------------------------------------------------------------------------------------|
| 0          | 10/31/22 | N/A        | Original Report Issue                                                                             |
| 1          | 12/12/22 | 1          | Updated to new company address                                                                    |
|            |          | 4          | Updated Section 4 information to specify the conditioning burn was performed at a medium setting. |
| 2          | 11/09/23 | Appendix F | Updated Appendix F to identify medium burn setting used for the conditioning burn.                |